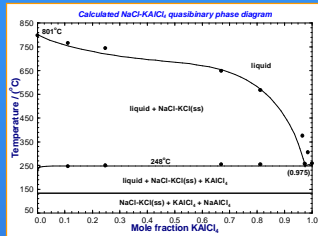
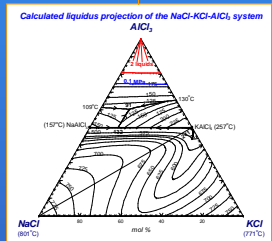


In ALL figures :
- the LINES are CALCULATED from the models
- the POINTS are EXPERIMENTAL from the literature

NaCl-KCl-AlCl₃ System (NO ternary parameters)

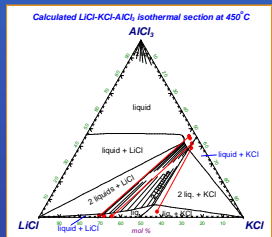


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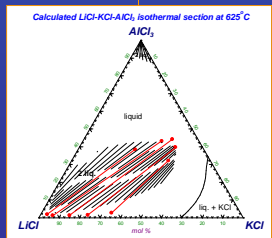


7

LiCl-KCl-AlCl₃ System (2 ternary parameters)



8



9

SUMMARY

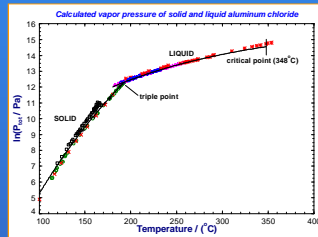
Chloroaluminate melts may be used as electrolytes for the production of aluminum and they are also involved in high energy density batteries ("Zebra" battery) : Na⁺-Al₂O₃/NaAlCl₄-FeCl₂-Fe.

Recently, the thermodynamic database previously developed [1,2a,2b] for the LiCl-NaCl-KCl-MgCl₂-CaCl₂-MnCl₂-FeCl₂-FeCl₃-CoCl₂-NiCl₂ system was extended with the addition of AlCl₃ and the thermodynamic "optimization" of the NaCl-KCl-AlCl₃ system was published [3]. In a thermodynamic "optimization" of a system, all available phase diagram and thermodynamic data (enthalpy of mixing, emf, vapor pressure measurements,...) are critically evaluated simultaneously in order to obtain one set of model equations for the Gibbs free energies of all phases (liquid, solid solutions, stoichiometric compounds) as functions of temperature and composition. From these equations, all of the thermodynamic properties and the phase diagrams can be back-calculated using Gibbs free energy minimization software. In this way, the data are rendered self-consistent, discrepancies among the data are identified, and extrapolations and interpolations are performed. The model parameters are stored in a computer database and the calculation of thermodynamic properties and phase diagram sections can be made over extended ranges of temperature and pressure.

In this work, all binary subsystems of the LiCl-NaCl-KCl-MgCl₂-CaCl₂-MnCl₂-FeCl₂-FeCl₃-CoCl₂-NiCl₂-AlCl₃ system (except AlCl₃-FeCl₃, for which 2 ternary solid solutions remain to be optimized) as well as all higher order (mostly ternary) subsystems for which experimental data were available have been considered. In particular, a thermodynamic modeling of the binary systems AlCl₃-AlCl₃ (where A = Li, Na and K) as a real challenge as these systems show strong negative deviations from ideality at the equimolar composition (due to short-range ordering in the liquid phase). This is illustrated for instance by the very steep NaCl liquidus in the calculated NaCl-AlCl₃ phase diagram (Figure 1) and by the rapid change in activity of AlCl₃ in the NaCl-AlCl₃ liquid (Figure 4).

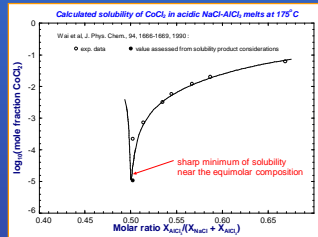
- [1] P. Chartrand and A.D. Pelton, *Metal. Mater. Trans.*, 2001, vol. 32A, pp. 1361-83.
[2a,2b] C. Robelin, P. Chartrand and A.D. Pelton, *J. Chem. Thermodyn.* (in press).
[3] C. Robelin, P. Chartrand and A.D. Pelton, *J. Chem. Thermodyn.*, 2004, vol. 36(8), pp. 683-99.

Pure Aluminum Chloride



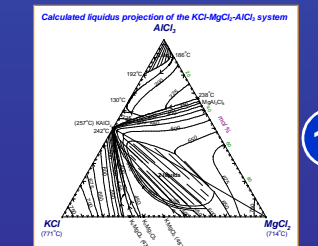
2

NaCl-CoCl₂-AlCl₃ System (NO ternary parameters)

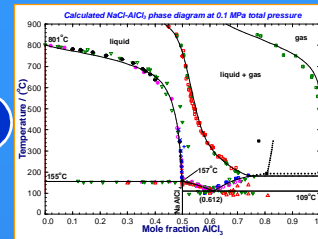


10

KCl-MgCl₂-AlCl₃ System (NO ternary parameters)

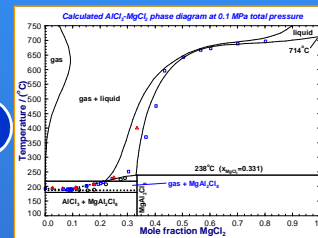


11



1

AlCl₃-MgCl₂ System



3

MODEL FOR THE LIQUID PHASE

The liquid solution was modeled using the Modified Quasichemical Model [4,5] which takes into account short-range ordering between second-nearest-neighbor cations (the anionic sublattices is occupied only by Cl ions). The parameters of the model are the Gibbs free energy changes $\Delta G_{i,j,k}$ for the following pair exchange reactions:



where A and B are two different cations. As $\Delta G_{i,j,k}$ becomes progressively more negative, reaction (1) is shifted to the right, (A-Cl-B) pairs predominate, and the solution becomes progressively more ordered. The Gibbs free energy of the liquid solution is given by:

$$G = \sum n_i \cdot g_i^* - T \cdot \Delta S^{conf} + \sum \sum n_{ij} (\Delta G_{ij}) \quad (2)$$

where n_i and g_i are the number of moles and molar Gibbs free energy of pure component i , ΔS^{conf} is an approximate expression for the configurational entropy of mixing, given by randomly mixing the (i-j) pairs, and n_{ij} is the number of moles of (i-j) pairs.

The binary systems AlCl₃-AlCl₃ (where A = Li, Na and K) show strong negative deviations from ideality at the equimolar composition (due to short-range ordering in the liquid phase), and the binary mixtures exhibit a region of liquid-liquid immiscibility at high AlCl₃ content (see the calculated NaCl-AlCl₃ phase diagram in Figure 1). The existence in AlCl₃-AlCl₃ melts of AlCl₂⁺ and Al₂Cl₇⁻ species has been observed by Raman spectroscopy [6,7]. The Modified Quasichemical Model does not explicitly introduce complex anions. However, short-range ordering through reaction (1) when $\Delta G_{i,j,k}$ is very negative is conceptually identical to the explicit assumption of complex anions and yields a very similar configurational entropy expression. In order to introduce two different compositions of maximum short-range-ordering near the AlCl₃ and Al₂Cl₇ compositions, pure liquid aluminum chloride was modeled as a mixture of AlCl₃ and Al₂Cl₇ (with paired aluminum cations) with the constraint that the experimental solid-liquid and liquid-gas equilibria be satisfactorily reproduced (Figure 2). The "AlCl₃-MCl₂" systems (where M = Mg, Mn, Fe, Co and Ni) were modeled by introducing two different compositions of maximum short-range-ordering near the MAl₂Cl₇ and MAl₃Cl₅ compositions (see the calculated AlCl₃-MgCl₂ phase diagram in Figure 3). Other results for the NaCl-AlCl₃ system are shown in Figures 4 & 5. Results for various multicomponent systems are shown in Figures 6, 7, 8, 9, 10, 11 & 12.

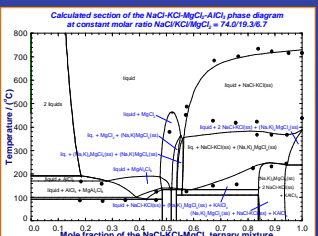
[4] A.D. Pelton, S.A. Degerterov, G. Eriksson, C. Robelin and Y. Dessureault, *Metal. Mater. Trans.*, 2000, vol. 31B, pp. 651-9.

[5] A.D. Pelton and P. Chartrand, *Metal. Mater. Trans.*, 2001, vol. 32A, pp. 1355-60.

[6] S.J. Cywin, P. Klaeboe, E. Rytter and H.A. Oye, *J. Chem. Phys.*, 1970, vol. 52, pp. 2776-8.

[7] H.A. Oye, E. Rytter, P. Klaeboe and S.J. Cywin, *Acta Chem. Scand.*, 1971, vol. 25, pp. 559-76.

NaCl-KCl-MgCl₂-AlCl₃ System



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